

Time-Domain Analysis of Control Systems

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Time Response

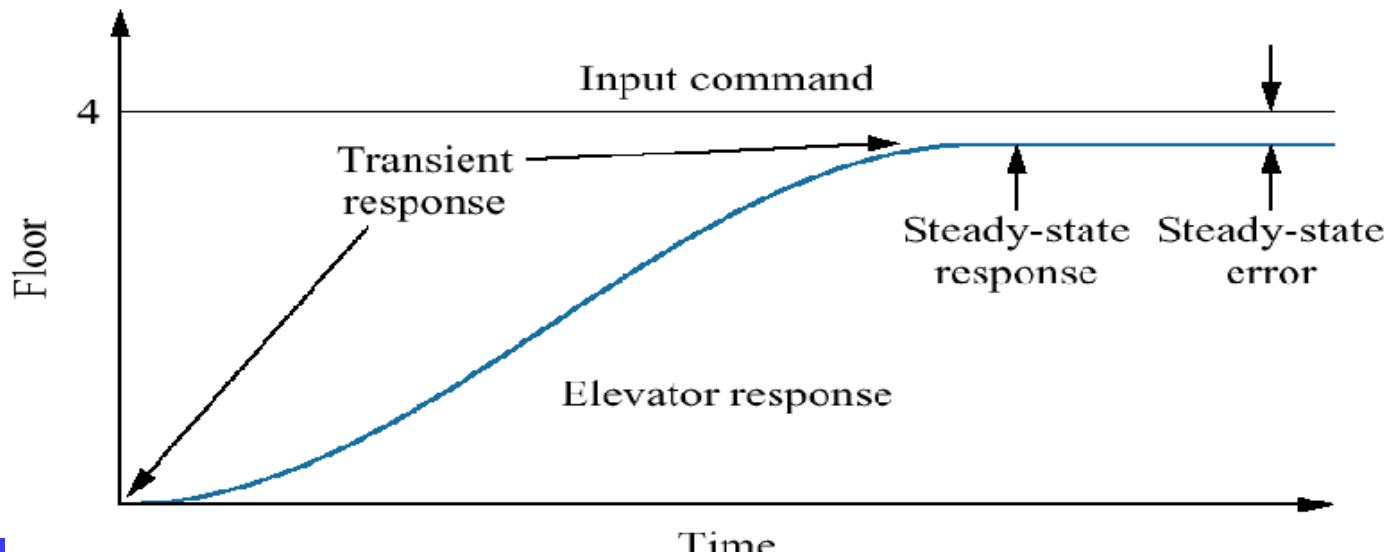
❑ Transient response

- Gradual change of the response from its initial state

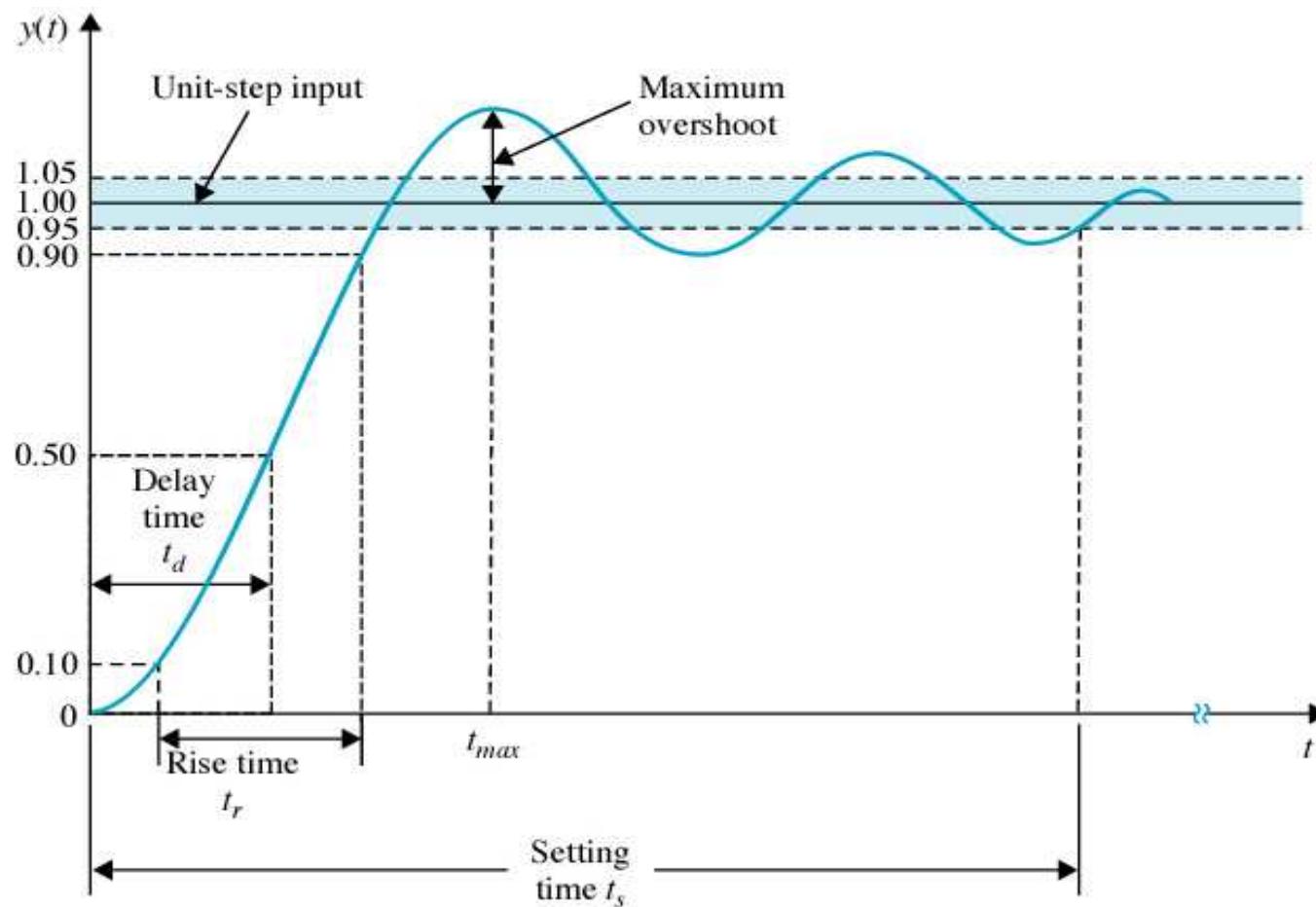
❑ Steady-state response

- Approximation to the desired response
- Steady-state error

- $e_{ss} = \text{Desired response} - \text{Steady-state response}$

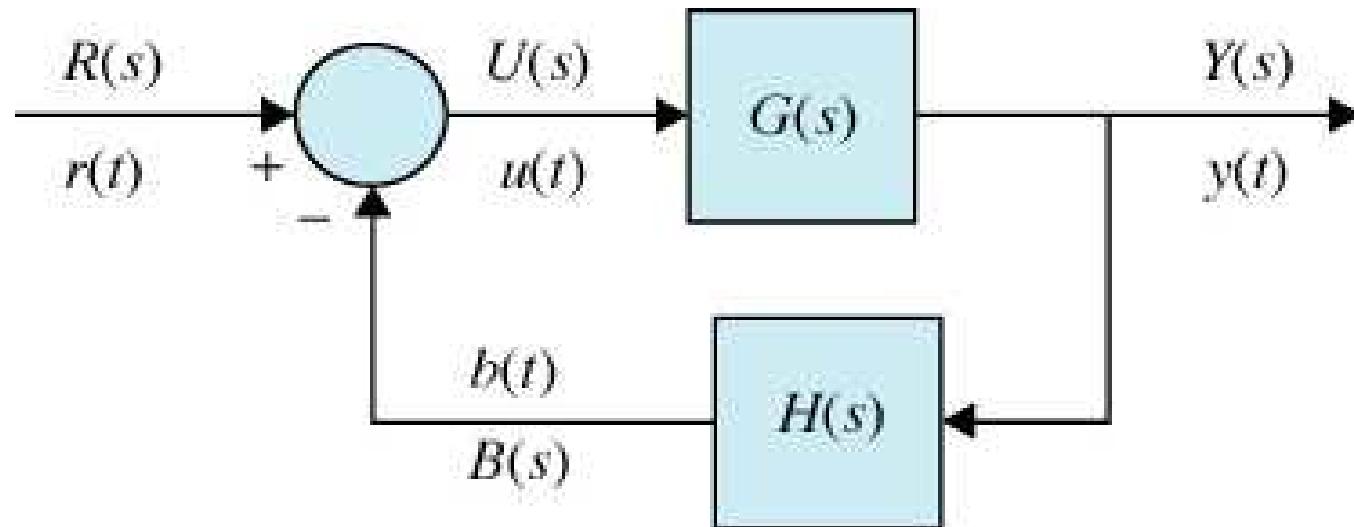


Unit Step Response & Time Domain Specs



Steady-State Error

- Error : $e(t) = r(t) - y(t)$
- Steady State Error : $e_{ss} = \lim_{t \rightarrow \infty} e(t) = \lim_{s \rightarrow 0} E(s)$



Type of Control Systems

- Steady State Error :

$$e(\infty) = \lim_{s \rightarrow 0} sE(s) = \lim_{s \rightarrow 0} \frac{sR(s)}{1 + G(s)H(s)}$$

- System Type : The number of poles of $G(s)H(s)$ at $s=0$

$$G(s)H(s) = \frac{(s+z_1)(s+z_2)\cdots}{s^n(s+p_1)(s+p_2)\cdots}$$

Step Error Constant

■ Steady State Error for Unit Step Function

$$e(\infty) = \lim_{s \rightarrow 0} \frac{sR(s)}{1 + G(s)H(s)} = \lim_{s \rightarrow 0} \frac{R}{1 + G(s)H(s)} = \frac{R}{1 + \lim_{s \rightarrow 0} G(s)H(s)}$$

■ Step Error Constant : K_p

$$K_p = \lim_{s \rightarrow 0} G(s)H(s)$$

- Type 0 : $e_{ss} = \frac{R}{1 + Kp}$
- Type 1 : $e_{ss} = 0$ since $Kp = \infty$

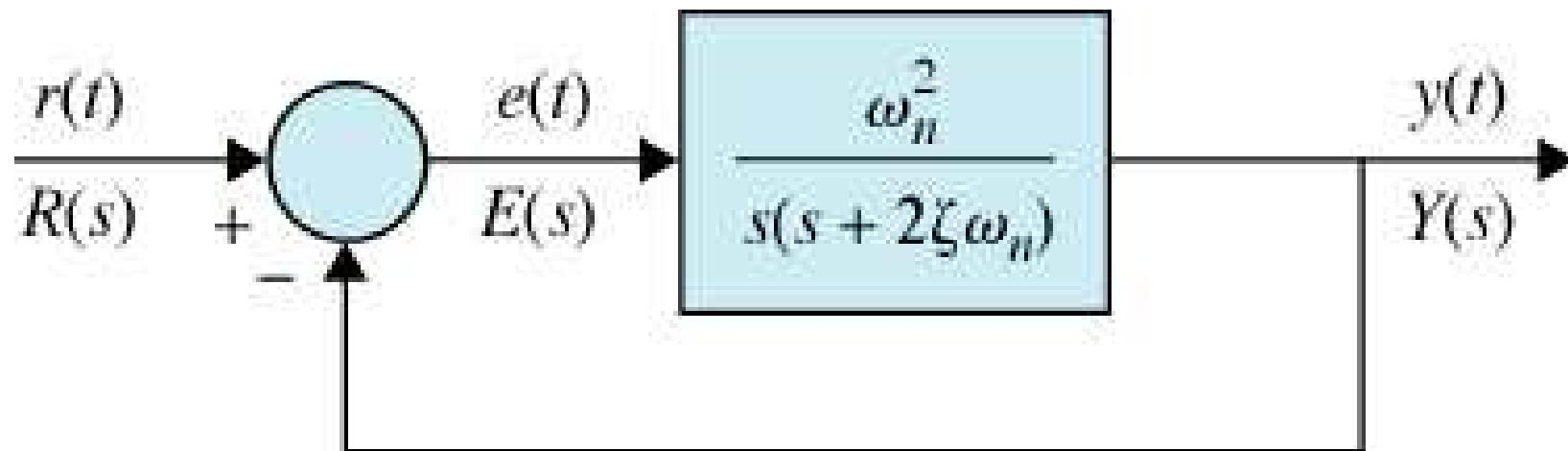
7-6. Second-Order System

■ Second-Order System

$$G(s) = \frac{Y(s)}{R(s)} = \frac{\omega_n^2}{s^2 + 2\zeta\omega_n s + \omega_n^2}$$

■ Example : RLC Circuit

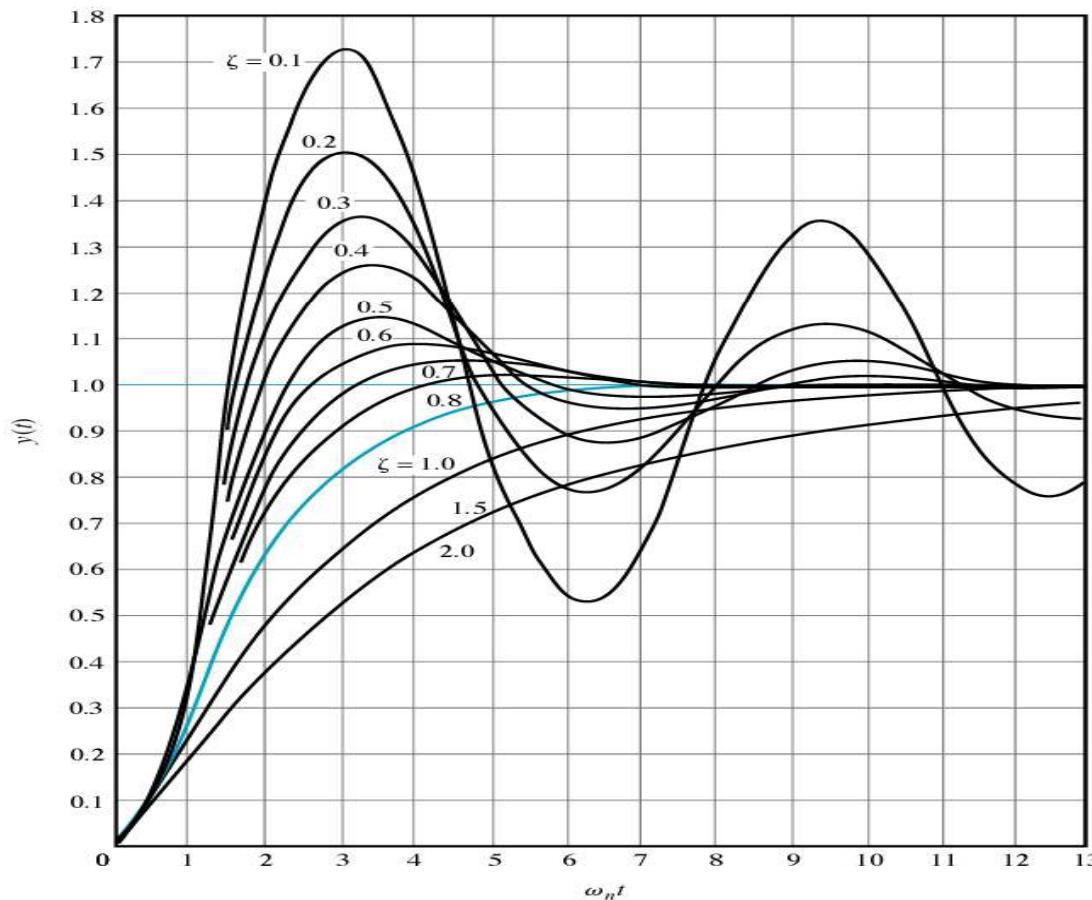
$$LC \frac{d^2v_c(t)}{dt^2} + RC \frac{dv_c(t)}{dt} + v_c(t) = v_s(t) \quad (LCs^2 + RCs + 1)V_c(s) = V(s)$$



Unit Step Response

■ Poles : $s = -\xi\omega_n \pm j\omega_n\sqrt{1-\xi^2}$

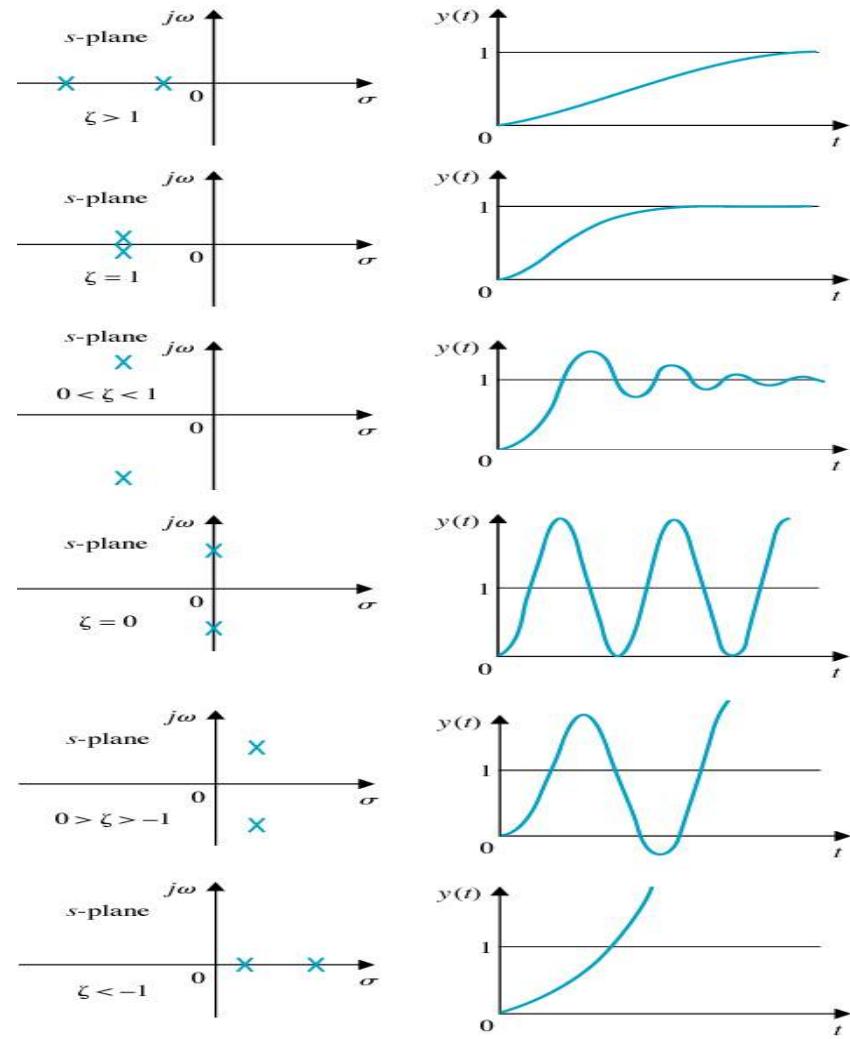
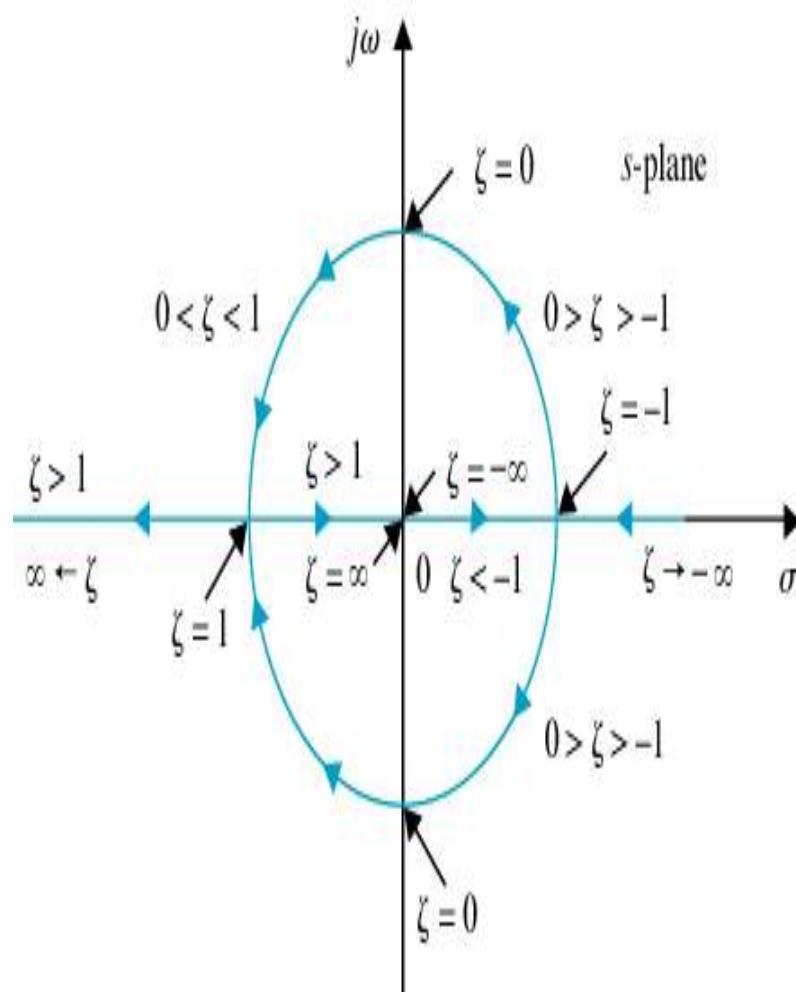
$$= -\sigma \pm j\omega$$



Damping

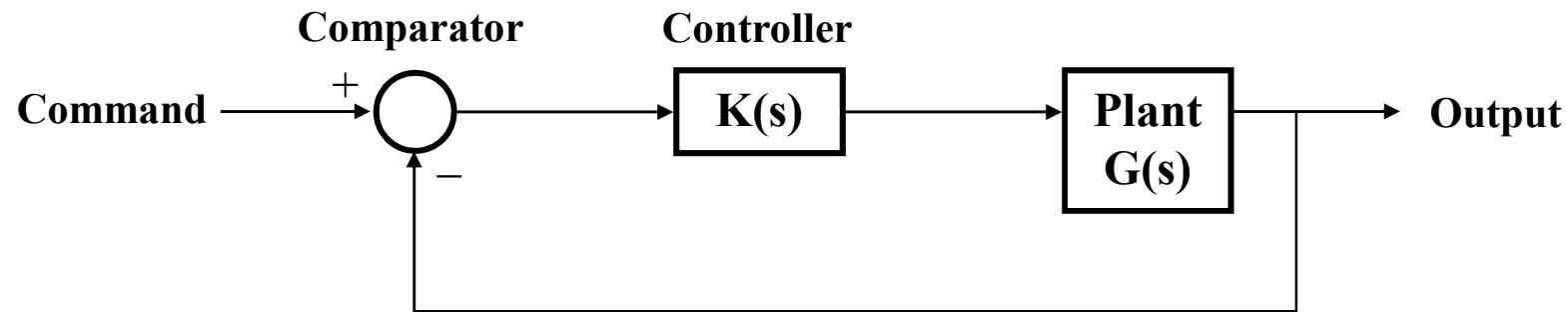
- Damping Factor : $\xi\omega_n$
- Damping : Damping ratio ξ
 - Overdamping : $\xi > 1$
 - Critical damping : $\xi = 1$
 - Underdamping : $\xi < 1$

Relation between System Poles & Response



Control System Block Diagram

- Control system block diagram



How to implement

- (1) Comparator ?
- (2) Controller ?

Control System Example

■ TE cooler

- It converts the electrical energy to thermal energy.
- Model

$$\frac{dT}{dt} = -k(T(t) - T_i(t) - T_a(t))$$

- Laplace Trasform

$$sT(s) - T(0) = -k T(s) + k T_i(s) + k T_a(s)$$

- Transfer function of TE Cooler : $T_a = 0$

$$G(s) = T(s)/T_i(s) = k/(s+k)$$

TEC Control

- Feedback Control : PI (Proportional & Integral) Control

$$T_i(t) = k_p(T(t) - T_s) + k_i \int_0^t (T(t) - T_s) dt$$

- Transfer Function of PI Control

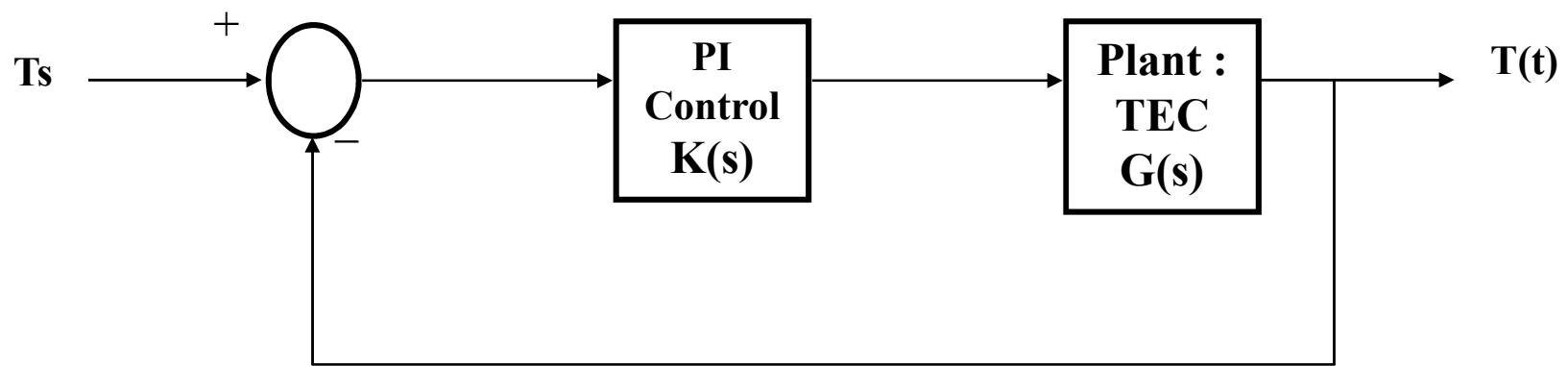
$$\begin{aligned} K(s) &= \frac{T_i(s)}{E(s)} \\ &= k_p + \frac{k_i}{s} \end{aligned}$$

where $E(s)$ is the Laplace transform of the error,

$$e(t) = T(t) - T_s.$$

Closed-Loop Transfer Function for TEC Control

■ Block Diagram



■ Closed-Loop Transfer Function

$$\begin{aligned} G_{CL}(s) &= \frac{T(s)}{T_s(s)} \\ &= \frac{G(s)K(s)}{1 + G(S)K(s)} \\ &= \frac{k(k_p s + k_i)}{s^2 + k(1 + k_p)s + kk_i} \end{aligned}$$